1. Plane Couette flow

Consider fluid between parallel planes. The wall at $y = 0$ is fixed, and the wall at $y = a$ moves with steady speed V in its own plane. Solve the Navier-Stokes equations for the case $\rho = constant$ to show that a possible flow is

$$
\mathbf{v} = \frac{Vy}{a}\mathbf{i}.
$$

Calculate the stress on both walls.

Solution:

Modeling: An obvious choice for the velocity field of the fluid is $\mathbf{v} = \mathbf{v}(y) = U(y)\mathbf{i}$. The inner pressure of the fluid is assumed constant, thus $\nabla p = 0$. Also it is assumed that no volume forces are present: $\rho f = 0$. The situation also seems to be static so that partial derivative of the velocity vanishes: $\partial \mathbf{v}/\partial t = 0$.

Figure 1: Schematics of the plane Couette flow: The lower boundary is fixed and the upper boundary moves with velocity V to right.

Boundary conditions: The upper plane, at $y = a$, is moving to the direction of i with velocity V. The boundary condition for velocity of the fluid v at $y = a$ is then

$$
\boldsymbol{v}(y=a) = U(a)\boldsymbol{i} = V\boldsymbol{i}.
$$

This condition says that the upper wall sees the fluid at rest. The second boundary condition says that also the lower wall sees the fluid at rest:

$$
\boldsymbol{v}(y=0)=0.
$$

Solution: The equation of motion, that is, the Navier-Stokes equation, stands as

$$
\rho \frac{Dv}{Dt} = \rho \boldsymbol{f} - \nabla p + \mu \nabla^2 \boldsymbol{v}
$$

and reduces to the form

 $\rho(\boldsymbol{v}\cdot\nabla)\boldsymbol{v}=\mu\nabla^2\boldsymbol{v}$

from which one sees that the left hand side also vanishes since $\mathbf{v} \cdot \nabla \mathbf{v} = U(y) \partial U(y)/\partial x = 0$. The equation

$$
0 = \frac{\partial^2 U(y)}{\partial y^2}
$$

is solved with function $U(y) = Dy + E$. The second boundary condition reduces the solution to the form $U(y) = Dy$ and the first boundary condition further to the form

$$
\boldsymbol{v}(y) = U(y)\boldsymbol{i} = V\frac{y}{a}\boldsymbol{i}.
$$

Stress on the walls: The force per area unit, stress, is calculated from the stress tensor

$$
\frac{dF_i}{dS} = \sigma_{ij} n_j,
$$

where n_j is the normal vector of the surface. The stress tensor

$$
\sigma_{ij} = -p\delta_{ij} + \sigma'_{ij}
$$

= $-p\delta_{ij} + \mu \left(\frac{\partial v_i}{\partial x_j} + \frac{\partial v_j}{\partial x_i} - \frac{2}{3} \delta_{ij} \frac{v_k}{x_k} \right) + K \delta_{ij} \frac{v_k}{x_k},$

which is just

$$
\sigma_{ij} = -p\delta_{ij} + \mu \frac{V}{a} (\delta_{i2}\delta_{j1} + \delta_{i1}\delta_{j2}).
$$

The surface normal points towards the fluid: at the upper to negative y direction $\hat{\mathbf{n}}^{\uparrow} = -\hat{\mathbf{j}}$ and at the lower plane to positive y direction $\hat{\mathbf{n}}^{\downarrow} = \mathbf{j}$. Thus the stress is

$$
\frac{dF_x}{dS} = \pm \sigma_{xy} n_y = \pm \mu \frac{V}{a}
$$
\n
$$
\frac{dF_y}{dS} = \pm \sigma_{yy} n_y = \pm p
$$

(upper sign for upper plane).

2. Flow down a slope (solving this problem gives double points)

A liquid of constant density flows down a plane which slopes at angle α to the horizontal, as indicated in the figure below. The free surface of the liquid is at a uniform distance from the plane, has pressure p_0 and no shear stress. For this flow you need to keep the gravitational field in the Navier-Stokes equation, as it is now dynamically active. Set up and solve equations for $U(y)$, and verify that the forces on a length l of the fluid layer are in equilibrium.

Solution:

Modeling: We have an equilibrium situation, where the fluid velocity $\mathbf{v} = U(y)\mathbf{i}$ and it does not change in time. The gravitational acceleration in the chosen coordinate system is

$$
\mathbf{g} = g(\mathbf{i}\sin\alpha - \mathbf{j}\cos\alpha),
$$

whose x-component is responsible for the motion of the fluid, while the y-component generates the hydrostatic pressure as we'll see soon. It is not applied external pressure

Figure 2: Schematics of the flow down a slope

gradient over the free ends of the liquid, so the pressure varies only in the y-direction such that $p(h) = p_0$, where h is the height of the fluid layer.

Solution of the Navier-Stokes equation: Using $f = g$, the full Navier-Stokes equation

$$
\rho \frac{Dv}{Dt} = \rho \mathbf{f} - \nabla p + \mu \nabla^2 \mathbf{v}
$$

reduces to the equilibrium condition in tha y - and x direction

$$
-\rho g \cos \alpha = \frac{\partial p}{\partial y},\tag{1}
$$

$$
0 = \rho g \sin \alpha - \frac{\partial p}{\partial x} + \mu \frac{\partial^2 U(y)}{\partial y^2}
$$
 (2)

Now there is no pressure gradient in x-direction, so $\partial p/\partial x = 0$. The pressure on the free surface of the fluid is just the air pressure $p(y = h) = p_0$. Integrating eq. (1), we get

$$
p(y) = -\rho g \cos \alpha y + a,
$$

and from the boundary condition $p(h) = p_0$ we get $a = p_0 + \rho g \cos \alpha h$. The pressure is

$$
p = \rho g \cos \alpha (h - y) + p_0. \tag{3}
$$

From eq. (2) , we now get

$$
-\rho g \sin \alpha = \mu \frac{\partial^2 U}{\partial y^2} \Rightarrow U(y) = -\frac{\rho g \sin \alpha}{2\mu} y^2 + by + c,
$$

where b and c are integration constants, which can be identified from the boundary conditions. On the solid surface the fluid velocity is zero, $U(0) = 0$, implying $c = 0$. On the free surface there is no shear stress apart from the pressure p_0 , so $\sigma_{xy} = 0$ at $y = h$, from which we get the second condition for the velocity. From the expression

$$
\sigma_{xy} = \mu \left(\frac{\partial U}{\partial y} \right) = -\rho g \sin \alpha y + \mu b
$$

we find at $y = h$ that

$$
b = \frac{-\rho g \sin \alpha h}{\mu}.
$$

Finally:

$$
U(y) = \frac{\rho g \sin \alpha}{2\mu} (2hy - y^2).
$$

The velocity field $U(y)$ is analogous to the fluid flow between walls, that is, to the example 7.1 of the lectures. Now, the velcity profile is parabolic, $\rho q \sin \alpha$ acts as an pressure gradient and the smaller viscosity μ the faster flow on the tilted plane.

Force balance: Next, we will verify that the forces on a portion of fluid, sketched in Fig. 2, are in equilibrium. We consider a volume $V = lwh$, where l is the length, w the width, and h the height of the fluid. The gravitation is the only volume force acting to this fluid element:

$$
\boldsymbol{F}^{(V)}=V\boldsymbol{f}=lwh\boldsymbol{g}.
$$

The second class of forces are the shear (surface) forces. Thus, we use the equation $dF_i = \sigma_{ii} n_i dS$ for the force on the fluid element due to the stress tensor. The normal vectors point out of the fluid element. Now, the components of the stress tensor are

$$
\sigma_{xy} = \rho g \sin \alpha (h - y) \qquad \qquad \sigma_{xx} = \sigma_{yy} = -p = -\rho g \cos \alpha (h - y) - p_0
$$

We first calculate the surface forces acting on the boundaries (1) and (3) of the fluid element, shown in Fig. 2.

First for the boundary (1), the surface element is now $dS_j = -wdy \delta_{xj}$ and thus the force

$$
\boldsymbol{F}^{(1)} = \int_{S_1} \boldsymbol{i} \sigma_{xk} \mathrm{d}S_k + \int_{S_1} \boldsymbol{j} \sigma_{yk} \mathrm{d}S_k = \int_0^h \boldsymbol{i} \sigma_{xx}(y) (-w \mathrm{d}y) + \int_0^h \boldsymbol{j} \sigma_{yx}(y) (-w \mathrm{d}y).
$$

For the boundary (3), the surface element points to the opposite direction $(dS_j = w dy \delta_{xj})$ but otherwise the expression for the force is the same, that is, $\mathbf{F}^{(3)} = -\mathbf{F}^{(1)}$. At the topmost surface, the shear stress vanishes ($\sigma_{xy} = 0$) and it acts only the air pressure

$$
\boldsymbol{F}^{(2)} = -lwp_0\boldsymbol{j}.
$$

The force on the fluid volume through the solid surface (4) is

$$
\boldsymbol{F}^{(4)} = \boldsymbol{j}\sigma_{yy}(y=0)(-lw) + \boldsymbol{i}\sigma_{xy}(y=0)(-lw) = lw(p_0 + hg\rho\cos\alpha)\boldsymbol{j} - lw\rho g\sin\alpha\boldsymbol{i}
$$

The total force acting through the surfaces is sum over all the surface forces yielding

$$
\boldsymbol{F}^{(S)} = \sum_{k=1}^{4} \boldsymbol{F}^{(k)} = lwh\rho(-\sin \alpha g \boldsymbol{i} + \cos \alpha g \boldsymbol{j}) = -lwh\rho \boldsymbol{g}.
$$

Finally, we see that the volume forces are balanced by the surface forces

$$
\boldsymbol{F} = \boldsymbol{F}^{(V)} + \boldsymbol{F}^{(S)} = 0
$$

Thus, the flow is static.